

Transport coefficients for suspensions of spherical particles

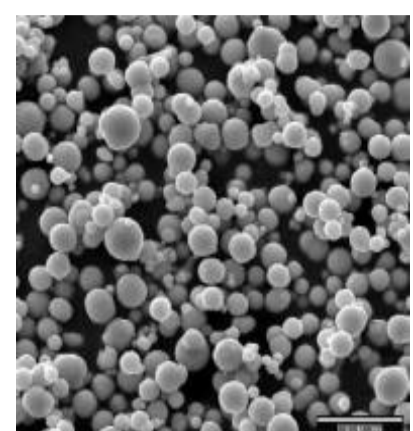
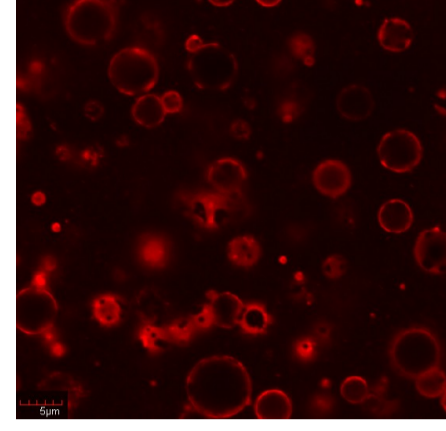
Karol Makuch, Bogdan Cichocki

Institute of Theoretical Physics, University of Warsaw, Poland



Motivation and aims

Suspensions in nature and industry



Micro:

Radius of particles
Viscosity of fluid
Number density of particles

Macroscopic properties:

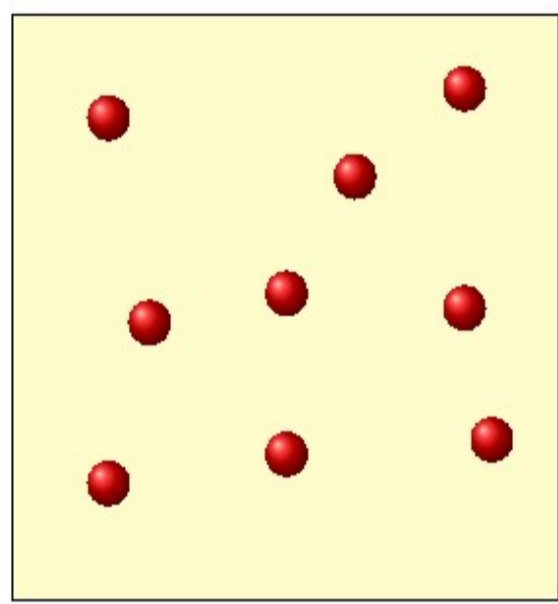
Effective viscosity
Sedimentation coefficient
Hydrodynamic factor

"The simplest" system: Suspension of spherical particles (hard spheres)

Problem: from micro to macro

Hard spheres suspension – microscopic description

Unbounded liquid,
N particles



Forces acting on suspension: $\mathbf{F}_0(\mathbf{r})$ (fluid), $\mathbf{F}_{\text{part}}(\mathbf{r})$ (particles)

Response of suspension: $\mathbf{v}_i, \Omega_i, \sum_{i=1}^N \mathbf{F}_i(\mathbf{r})$ (translational and angular velocity, surface forces)

Stokes equations:

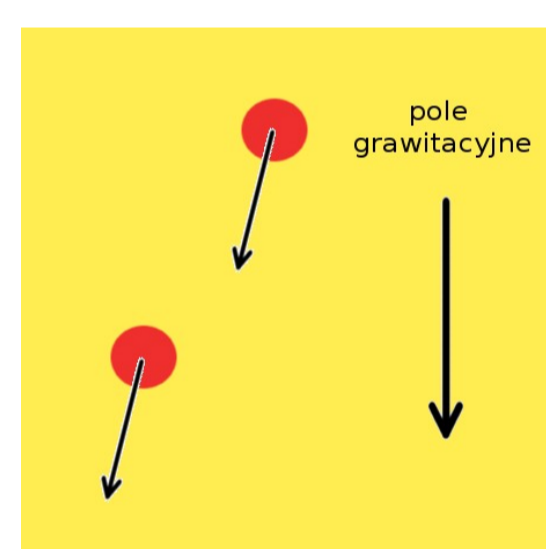
$$\nabla p(\mathbf{r}) - \eta \Delta \mathbf{v}(\mathbf{r}) = \mathbf{F}_0(\mathbf{r}) + \sum_{i=1}^N \mathbf{F}_i(\mathbf{r})$$

$$\nabla \cdot \mathbf{v}(\mathbf{r}) = 0$$

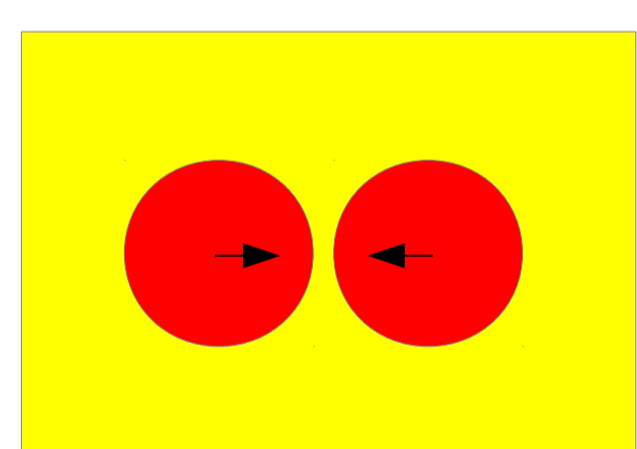
Hydrodynamic interactions

Three important features of hydrodynamic interactions:

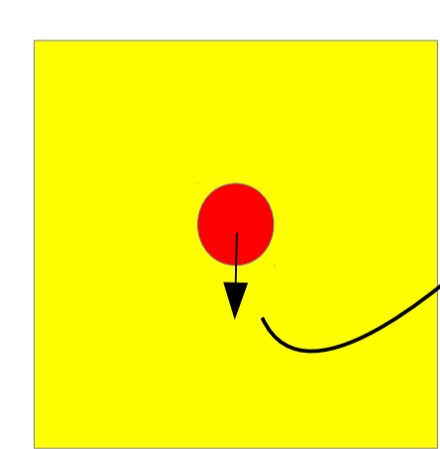
- strong interactions of close particles
- long-range
- many-body



For constant velocities asymptotically infinite drag force:



Slow decreasing of velocity field around sedimenting single particle:



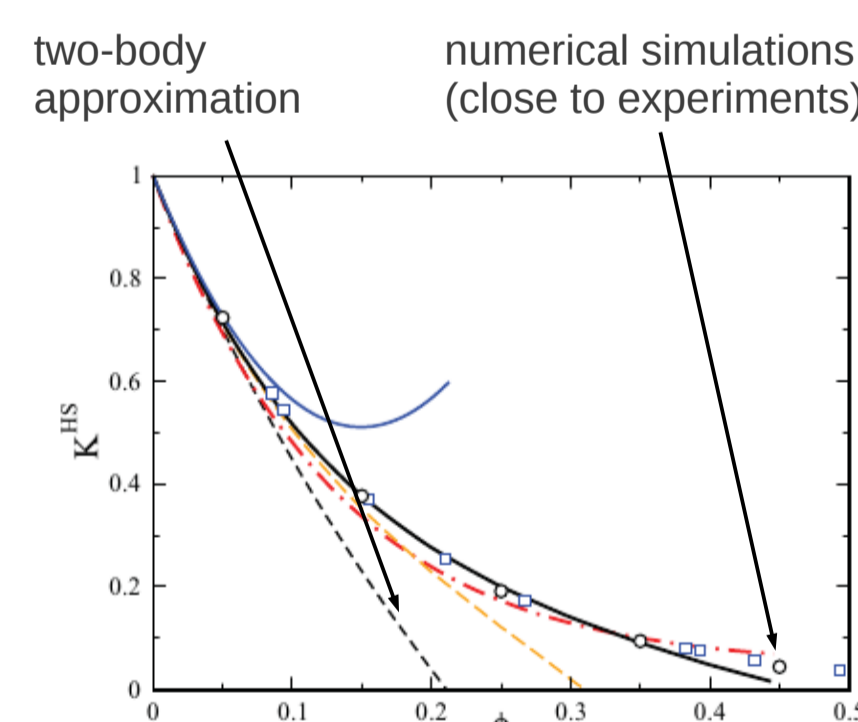
$$\mathbf{v}(\mathbf{r}) \sim \mathbf{G}(\mathbf{r}) \cdot \mathbf{F}$$

Oseen tensor:

$$\mathbf{G}(\mathbf{r}) = \frac{1}{8\pi\eta} \frac{\mathbf{1} + \hat{\mathbf{r}}\hat{\mathbf{r}}}{r}$$

Integral over r not absolutely convergent

Many-body character:



M. Heinen, A. Banchio, and G. Nägele, J. Chem. Phys. 135, 154504 (2011).

Single particle in ambient flow:

$$\mathbf{v}_0(\mathbf{r}) = \int d^3r' \mathbf{G}(\mathbf{r} - \mathbf{r}') \cdot \mathbf{f}_0(\mathbf{r}')$$

$$\mathbf{f}_1(\mathbf{r}) = \int d\mathbf{r}' \mathbf{M}(\mathbf{r} - \mathbf{R}_1, \mathbf{r}' - \mathbf{R}_1) \mathbf{v}_0(\mathbf{r}')$$

Single freely moving particle response operator

Suspension in ambient flow:

$$\mathbf{f}_i = \mathbf{M}(i) \left(\mathbf{v}_0 + \sum_{j \neq i} \mathbf{G}\mathbf{f}_j \right)$$

Scattering series

$$\mathbf{f}_i = \left(\mathbf{M}(i) + \sum_{j \neq i} \mathbf{M}(i)\mathbf{G}\mathbf{M}(j) + \sum_{j \neq i, k \neq j} \mathbf{M}(i)\mathbf{G}\mathbf{M}(j)\mathbf{G}\mathbf{M}(k) + \dots \right) \mathbf{v}_0$$

Green function for Stokes equations

$$M(1)\mathbf{G}M(3)\mathbf{G}M(2)\mathbf{G}M(1) \times G \times M(4)\mathbf{G}M(5)\mathbf{G}M(4) \times G \times M(6)$$

short range hydrodynamic interactions (strong interactions of close particles)

long range hydrodynamic interactions (nodal line)

block structure:

$$S_I(C_1) \text{---} S_I(C_2) \text{---} S_I(C_3)$$

$$C_1 \equiv 123 \quad C_2 \equiv 45 \quad C_3 \equiv 6$$

Macroscopic description

Average force density:

$$\langle f(\mathbf{R}) \rangle \equiv \left\langle \sum_i f_i \delta(\mathbf{R} - \mathbf{i}) \right\rangle$$

Average over probability distribution for configurations of particles, thermodynamic limit

$$\langle f(\mathbf{R}) \rangle = \int d^3\mathbf{R}' T(\mathbf{R}, \mathbf{R}') v_0(\mathbf{R}')$$

Response operator for suspension in ambient flow

$$T = \sum_{b=1}^{\infty} \sum_{C_1 \dots C_b} \int dC_1 \dots dC_b n(C_1 \dots C_b) S_I(C_1) G \dots G S_I(C_b)$$

s-particle distribution functions

Response of suspension (effective viscosity)

average velocity field of suspension

$$\langle f \rangle(\mathbf{R}) = \int d\mathbf{r}' T^{irr}(\mathbf{R}, \mathbf{r}') \langle v \rangle(\mathbf{r}')$$

average surface dipole force

$$\langle v(\mathbf{R}) \rangle = v_0(\mathbf{R}) + \int d\mathbf{r}' G(\mathbf{R}, \mathbf{r}') \langle f(\mathbf{r}') \rangle$$

Relation between T and T^{irr} operators:

$$T = T^{irr} (1 - G T^{irr})^{-1}$$

Felderhof, Ford, Cohen (1982):

$$T^{irr} = \sum_{g=1}^{\infty} \sum_{C_1 \dots C_g} \int dC_1 \dots dC_g b(C_1 | \dots | C_g) S_I(C_1) G \dots G S_I(C_g)$$

Effective viscosity coefficient is given directly by the response operator T^{irr}

$$b(C) = n(C)$$

$$b(C_1 | \dots | C_k | C_{k+1} | \dots | C_g) = b(C_1 | \dots | C_k C_{k+1} | \dots | C_g)$$

$$-b(C_1 | \dots | C_k) b(C_{k+1} | \dots | C_g)$$

Renormalization

Ring expansion (2011):

$$T^{irr} = \sum_{b=1}^{\infty} \sum_{C_1 \dots C_b} \int dC_1 \dots dC_b H(C_1 | \dots | C_b) S_I(C_1) G_{\text{eff}} \dots G_{\text{eff}} S_I(C_b)$$

Block correlation functions (recurrence formula):

$$b(C_1 | \dots | C_b) = \sum_{r=1}^{b-1} \sum_{1=i_1 < i_2 < \dots < i_{r+1}=b} H(C_{i_1} | \dots | C_{i_{r+1}}) n(\{C_{i_1} \dots C_{i_2}\} \setminus \{C_{i_1} C_{i_2}\}) \dots n(\{C_{i_r} \dots C_{i_{r+1}}\} \setminus \{C_{i_r} C_{i_{r+1}}\})$$

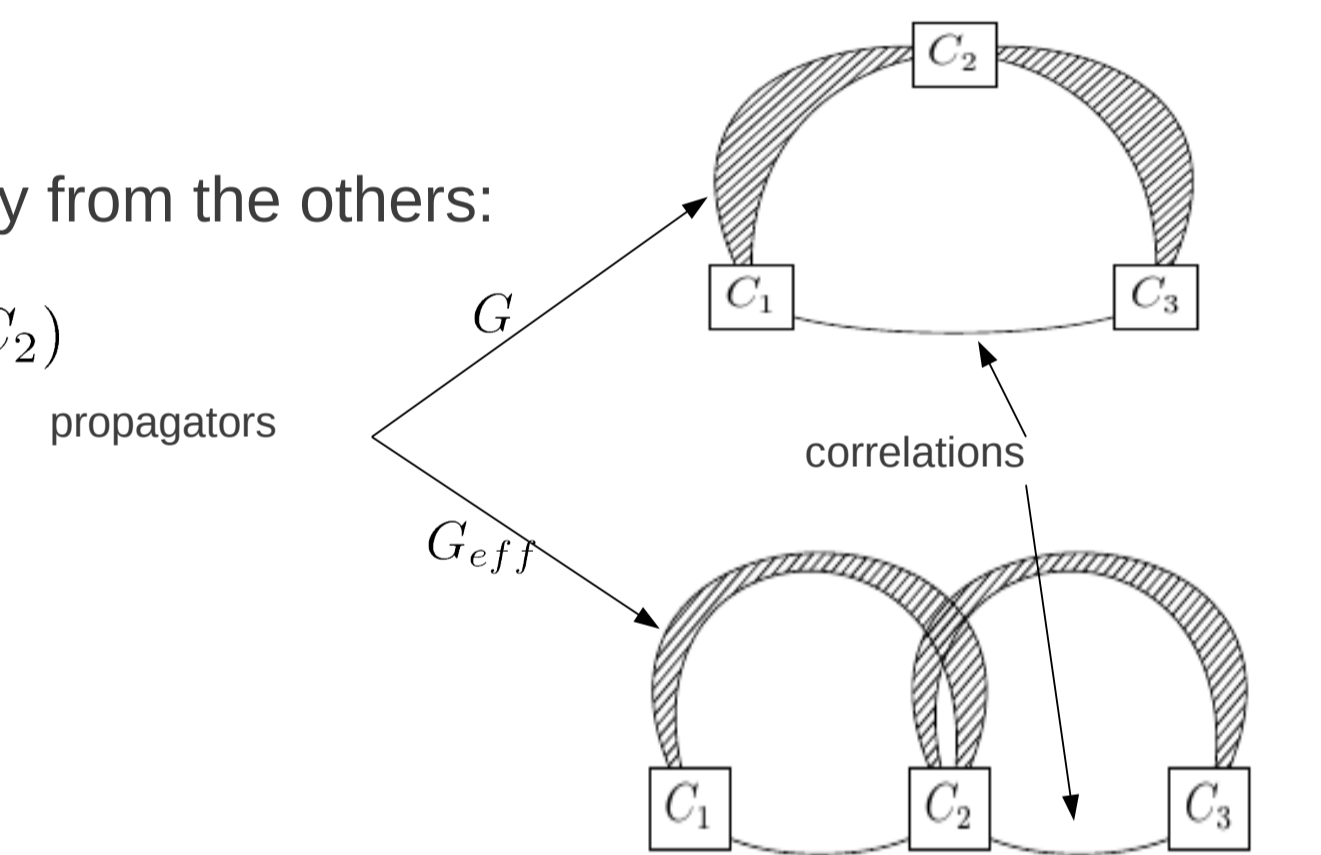
When the middle group goes away from the others:

Cluster expansion: $b(C_1 | C_2 | C_3) \rightarrow b(C_1 | C_3) b(C_2)$

Ring expansion: $H(C_1 | C_2 | C_3) \rightarrow 0$

Two important differences:

- propagator
- volume of integration



Approximate method of calculations of transport properties

Repeating structures in T^{irr}

Felderhof, Ford, Cohen (1982) (Mayer instead of h):

$$T^{irr} = T_{CM}^{irr} (1 - [hG] T_{CM}^{irr})^{-1}$$

Clausius-Mossotti operator

Clausius-Mossotti approximation:

$$T_{CM}^{irr} \approx nM$$

renormalized Clausius-Mossotti operator

$$T^{irr} = T_{RCM}^{irr} (1 - [hG_{\text{eff}}] T_{RCM}^{irr})^{-1}$$

Approximate method formulated in terms of approximation for T_{RCM}^{irr}
G ⇒ G_{eff}

Generalized Clausius-Mossotti approximation:

$$T_{RCM}^{irr} \approx nB$$

(two-body hydrodynamic interactions incomplete – the same as in δy scheme (1983))

One-ring approximation (fully takes into account two-body hydrodynamic interactions)

Input:
-volume fraction
-two-body correlation function (PY); (three-particle correlation function by two body correlation function (Kirkwood))
-two-body hydrodynamic interactions

